

Advanced Fluid Mechanics

Homework4

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Master on Numerical Methods in Engineering

Part one

(a) Considering that,

$$r^2 = x^2 + y^2$$

$$\tan(\theta) = \frac{y}{x}$$

We can rewrite the stream function in the following way,

$$\psi(x, y) = \psi(r, \theta) = Ur^2 \sin(2\theta) = 2Ur^2 \sin(\theta) \cos(\theta)$$

Hence, we get the stream function in Cartesian coordinates,

$$\psi(x, y) = 2U(x^2 + y^2) \frac{y}{\sqrt{x^2 + y^2}} \frac{x}{\sqrt{x^2 + y^2}} = 2Uxy$$

$$x - \text{component: } u = \frac{\partial \psi}{\partial y} = 2Ux$$

$$y - \text{component: } v = -\frac{\partial \psi}{\partial x} = -2Uy$$

It is clearly shown that at the point (0,0), the velocity is zero, so this point is a stagnation point.

Considering the boundary condition that,

$$u(x, 0) = 0$$

$$v(x, 0) = 0$$

So the x-component velocity does not satisfy the no-slip boundary condition, while the y-component velocity satisfies the boundary condition.

From the Bernoulli equation, the pressure distribution will be,

$$p = p_0 - 2\rho U^2(x^2 + y^2)$$

where p_0 is the Bernoulli constant that corresponds to the pressure at the stagnation point.

(b) Firstly, we write the N-S equations,

$$\begin{cases} \nabla \cdot \mathbf{v} = 0 \\ \mathbf{v}_t + (\mathbf{v} \cdot \nabla) \mathbf{v} - \nu \nabla^2 \mathbf{v} + \nabla P = \mathbf{0} \end{cases}$$

Substituting the known x,y-component to the N-S equations, we can get the follow equation,

$$\begin{cases} 0 = 0 \\ 4U^2x = 4U^2x \\ 4U^2y = 4U^2y \end{cases}$$

So this velocity and pressure distributions verify the N-S equations.

However, the viscous-shear terms in the Navier-Stokers equations are identically zero for the potential-flow fields, so it does not fulfill the boundary conditions for the viscous problem.

Advanced Fluid Mechanics

(c) Continuity equation,

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0$$

$$\frac{\partial v}{\partial y} = -\frac{\partial u}{\partial x} = -2Uf'(y)$$

So that the vertical component of the velocity will be of the form,

$$v = -2Uf(y)$$

Define the velocity field in this way enable all function $f(y)$ could satisfy the continuity equation. Considering the boundary condition, we stipulate that,

$$f(y) \rightarrow y \text{ as } y \rightarrow \infty$$

$$f(0) = f'(0) = 0$$

$$f'(y) \rightarrow 1 \text{ as } y \rightarrow \infty$$

(d) The y -momentum equation can be written,

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right)$$

Substituting the knowing results,

$$4U^2 f f' = -\frac{1}{\rho} \frac{\partial p}{\partial y} - 2U\nu f''$$

Hence, the pressure distribution,

$$p(x, y) = -2\rho U^2 f^2 - 2\rho U\nu f' + h(x)$$

where $h(x)$ is some function of x that may be determined by comparison with the potential-flow pressure distribution that should be recovered for large values of y . Since $f(y) \rightarrow y$ as $y \rightarrow \infty$,

$$p(x, y) \rightarrow -2\rho U^2 y^2 - 2\rho U\nu + h(x)$$

Recalling the in the previous (a), we have,

$$p(x, y) = p_0 - 2\rho U^2 (x^2 + y^2)$$

So compare the two pressure distribution,

$$h(x) = p_0 - 2\rho U^2 x^2 + 2\rho U\nu$$

The final pressure distribution should be,

$$p(x, y) = p_0 - 2\rho U^2 (f^2 + x^2) - 2\rho U\nu (f' - 1)$$

(e) Using the pressure distribution in (d),

$$\frac{\partial p}{\partial x} = -4\rho U^2 x$$

So that the x -momentum becomes,

$$4U^2 x (f')^2 - 4U^2 x f f'' = 4U^2 x + 2U\nu x f'''$$

Rewrite it in the following way,

$$\frac{\nu}{2U} f''' + f f'' - (f')^2 + 1 = 0$$

This is a three order differential equation with the boundary conditons,

$$f(y) \rightarrow y \text{ as } y \rightarrow \infty$$

Advanced Fluid Mechanics

$$f(0) = f'(0) = 0$$

$$f'(y) \rightarrow 1 \text{ as } y \rightarrow \infty$$

Part two

According to the boundary conditions:

$$u = 0 \text{ at } y = 0$$

$$u = U, \frac{\partial u}{\partial y} = 0 \text{ at } y = \delta$$

We can solve the quadratic polynomial equation,

$$\frac{u}{U} = a + b\frac{y}{\delta} + c\left(\frac{y}{\delta}\right)^2$$

that,

$$a = 0, b = 2, c = -1$$

Hence, the polynomial equation is,

$$\frac{u}{U} = 2\frac{y}{\delta} - \left(\frac{y}{\delta}\right)^2$$

Now in this case is an uniform flow over a flat plate, so the momentum integral equation is,

$$\frac{d}{dx} \int_0^{\infty} u(U - u)dy = \frac{\tau_0}{\rho}$$

Since,

$$\frac{\tau_0}{\rho} = \nu \frac{\partial u}{\partial y}(y = 0) = \frac{2\nu U}{\delta}$$

and the momentum thickness,

$$\theta = \int_0^{\delta} \frac{u}{U} \left(1 - \frac{u}{U}\right) dy = \frac{2}{15} \delta$$

Substituting in the momentum integral equation,

$$\frac{2}{15} U^2 \frac{d\delta}{dx} = \frac{2\nu U}{\delta}$$

By integration, we obtain,

$$\delta = 5.477 \sqrt{\frac{\nu x}{U}}$$

And,

$$\frac{\delta}{x} = \frac{5.477}{\sqrt{Re}}$$

As a comparison, the following table is shown,

Advanced Fluid Mechanics

	Blasius solution	Quadratic solution	Cubic solution
<i>thickness:</i> $\frac{\delta}{x}$	$\frac{5}{\sqrt{Re}}$	$\frac{5.477}{\sqrt{Re}}$	$\frac{4.64}{\sqrt{Re}}$
<i>momentum thickness:</i> $\frac{\theta}{x}$	$\frac{0.644}{\sqrt{Re}}$	$\frac{0.73}{\sqrt{Re}}$	$\frac{0.646}{\sqrt{Re}}$