## Homework 3 - AFM

## Bruno Aguirre, Lisandro Roldan

December 3, 2015

1 Considering the problem of long distance oil transport proposed in the assignment.

## 1.1 )

The relevant quantities that describe the problem are shown in the table bellow.

|  | $\frac{\Delta P}{L}\left[\frac{\mathrm{~kg}}{\mathrm{~m}^{2} s^{2}}\right]$ | $\rho\left[\frac{\mathrm{kg}}{\mathrm{m}^{3}}\right]$ | $v_{o}\left[\frac{\mathrm{~m}}{\mathrm{~s}}\right]$ | $R[\mathrm{~m}]$ | $R_{1}[\mathrm{~m}]$ | $\mu_{1}\left[\frac{\mathrm{~kg}}{\mathrm{~ms}}\right]$ | $\mu_{2}\left[\frac{\mathrm{~kg}}{\mathrm{~ms}}\right]$ | $\sigma\left[\frac{\mathrm{m}}{s^{2}}\right]$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| M | 1 | 1 | 0 | 0 | 0 | 1 | 1 | 1 |
| L | -2 | -3 | 1 | 1 | 1 | -1 | -1 | 0 |
| T | -2 | 0 | -1 | 0 | 0 | -1 | -1 | -2 |

With this data, the $\pi$-products can be calculated using $v_{0}, \rho$ and $R_{1}$ as primary variables as following:

$$
\begin{array}{ll}
\pi_{1}=\frac{\Delta P}{L} \rho^{a} v_{0}^{b} R_{1}^{c} & M L^{-2} T^{-2}\left(M L^{-3}\right)^{a}\left(L T^{-1}\right)^{b}(L)^{c}=M^{0} L^{0} T^{0} \\
& \pi_{1}=\frac{\Delta P}{L} \frac{R_{1}}{\rho v_{0}^{2}}
\end{array}
$$

$$
\pi_{2}=R \rho^{a} v_{0}^{b} R_{1}^{c}
$$

$$
M\left(M L^{-3}\right)^{a}\left(L T^{-1}\right)^{b}(L)^{c}=M^{0} L^{0} T^{0}
$$

$$
\pi_{2}=\frac{R}{R_{1}}
$$

$$
\pi_{3}=\mu_{1} \rho^{a} v_{0}^{b} R_{1}^{c}
$$

$$
M L^{-1} T^{-1}\left(M L^{-3}\right)^{a}\left(L T^{-1}\right)^{b}(L)^{c}=M^{0} L^{0} T^{0}
$$

$$
\pi_{3}=\frac{\mu_{1}}{\rho v_{0} R_{1}}
$$

$$
\pi_{4}=\mu_{2} \rho^{a} v_{0}^{b} R_{1}^{c}
$$

$$
M L^{-1} T^{-1}\left(M L^{-3}\right)^{a}\left(L T^{-1}\right)^{b}(L)^{c}=M^{0} L^{0} T^{0}
$$

$$
\pi_{4}=\frac{\mu_{2}}{\rho v_{0} R_{1}}
$$

$$
\pi_{5}=\sigma \rho^{a} v_{0}^{b} R_{1}^{c}
$$

$$
\begin{aligned}
& M T^{-2}\left(M L^{-3}\right)^{a}\left(L T^{-1}\right)^{b}(L)^{c}=M^{0} L^{0} T^{0} \\
& \pi_{5}=\frac{\sigma}{\rho v_{0}^{2} R_{1}}
\end{aligned}
$$

## 1.2 )

From the $\pi$-products acquired, we can see that $\pi_{2}, \pi_{3}$ and $\pi_{5}$ can be related to the Reynolds and Weber numbers as:

$$
R e_{1}=\frac{1}{\pi_{3}} \quad R e_{2}=\frac{1}{\pi_{4}} \quad W e=\frac{1}{\pi_{5}}
$$

Being the Reynolds and Weber numbers:

$$
R e=\frac{\rho V l}{\mu} \quad W e=\frac{\rho V^{2} l}{\sigma}
$$

Where $l$ and $V$ are respectively characteristic length and velocity. The Weber number is used in fluid flows when there is a interface between two different fluids, it measures the relative importance of the inertial forces compared to the surface tension. This quantity is important to determine whether waves will develop on the interface of fluids. In order to this waves not to form the tangential components $\sigma / R_{1}$ has to be bigger them the inertial component $v_{0} \rho$, in other words, $W e<1$ or $\pi_{5}>1$.

## 1.3 )

The hypothesis can be considered reasonable because both fluids present the same density. Gravity terms become important when density difference are significant, as it can be seem in another dimensionless number called Eotvos Number, which describes the possibility of wave formation in the interface between to fluids.

$$
E o=\frac{\Delta \rho g L^{2}}{\sigma}
$$

For the case presented, $\Delta \rho$ is equal to $0(E o=0)$ preventing the body forces (gravity) being sources of wave generation.

## 1.4 )

The Navier-Stokes equations written in cylindrical coordinates are presented bellow considering a velocity field on the form of $v=\left(0,0, v_{z}(r)\right)$.
$\rho\left(\frac{\partial v_{r}}{\partial t}+v_{r} \frac{\partial v_{r}}{\partial r}+\frac{v_{\theta}}{r} \frac{\partial v_{r}}{\partial \theta}-\frac{v_{\theta}^{2}}{r}+v_{z} \frac{\partial v_{r}}{\partial z}\right)=-\frac{\partial p}{\partial r}+\mu\left(\frac{\partial}{\partial r}\left(\frac{1}{r} \frac{\partial}{\partial r}\left(r v_{r}\right)\right)+\frac{1}{r^{2}} \frac{\partial^{2} v_{r}}{\partial \theta^{2}}-\frac{2}{r^{2}} \frac{\partial v_{\theta}}{\partial \theta}+\frac{\partial^{2} v_{r}}{\partial z^{2}}\right)+\rho b_{r}$
$\rho\left(\frac{\partial v_{\theta}}{\partial t}+v_{r} \frac{\partial v_{\theta}}{\partial r}+\frac{v_{\theta}}{r} \frac{\partial v_{\theta}}{\partial \theta}+\frac{v_{r} v_{\theta}}{r}+v_{z} \frac{\partial v_{\theta}}{\partial z}\right)=-\frac{1}{r} \frac{\partial p}{\partial \theta}+\mu\left(\frac{\partial}{\partial r}\left(\frac{1}{r} \frac{\partial}{\partial r}\left(r v_{\theta}\right)\right)+\frac{1}{r^{2}} \frac{\partial^{2} v_{\theta}}{\partial \theta^{2}}+\frac{2}{r^{2}} \frac{\partial v_{r}}{\partial \theta}+\frac{\partial^{2} v_{\theta}}{\partial z^{2}}\right)+\rho b_{\theta}$

$$
\rho\left(\frac{\partial v_{z}}{\partial t}+v_{r} \frac{\partial v_{z}}{\partial r}+\frac{v_{\theta} \partial v_{z}}{r} \frac{\partial v_{z}}{\partial \theta} \frac{\partial v_{z}}{\partial z}\right)=-\frac{\partial p}{\partial z}+\mu\left(\frac{1}{r} \frac{\partial}{\partial r}\left(r \frac{\partial v_{z}}{\partial r}\right)+\frac{1}{r^{2}} \frac{\partial^{2} v_{z}}{\partial \theta^{2}}+\frac{\partial^{2} v_{z}}{\partial z^{2}}\right)+\rho b_{z}
$$

The $r$ and $\theta$ components of the velocity, the derivatives $v_{z}$ with respect to $\theta$ and $z$, gravity terms and the $\theta$ and $r$ components of the pressure gradient are neglected (as it is stated in the problem). After the all the simplifications, the resulting equation is presented with its appropriate boundary conditions:

$$
\left\{\begin{array}{l}
\frac{1}{r} \frac{\partial}{\partial r}\left(r \frac{\partial v_{z}}{\partial r}\right)=-\frac{1}{\mu} \frac{\Delta P}{L} \\
v_{z}^{w}(R)=0 \\
v_{z}^{w}\left(R_{1}\right)=v_{z}^{o}\left(R_{1}\right) \\
\tau^{w}\left(R_{1}\right)=\tau^{o}\left(R_{1}\right) \\
\tau^{w}(0)=0
\end{array}\right.
$$

## 1.5 )

In order to solve this problem, its necessary to integrate the resulting equation twice as following:

$$
\frac{\partial v_{z}}{\partial r}=-\frac{r}{2 \mu} \frac{\Delta P}{L}+\frac{A}{r} \quad v_{z}=\frac{r^{2}}{4 \mu} \frac{\Delta P}{L}+A \ln (r)+B
$$

For oil $0 \leq r \leq R_{1}$ we have:

$$
v_{z}^{o}(r)=\frac{-r^{2}}{4 \mu_{1}} \frac{\Delta P}{L}+A \ln (r)+B \quad \tau^{o}(r)=\mu_{1} \frac{\partial v_{z}}{\partial r}=-\frac{r}{2} \frac{\Delta P}{L}+\frac{A \mu_{1}}{r}
$$

For water $R_{1} \leq r \leq R$ we have:

$$
v_{z}^{w}(r)=\frac{-r^{2}}{4 \mu_{2}} \frac{\Delta P}{L}+C \ln (r)+D \quad \tau^{w}(r)=\mu_{2} \frac{\delta v_{z}}{\delta r}=-\frac{r}{2} \frac{\Delta P}{L}+\frac{C \mu_{2}}{r}
$$

Now the boundary conditions are applied to find the integration constants:

$$
\begin{array}{llr}
\tau^{w}(0)=0 & \frac{A \mu_{1}}{0} \rightarrow \infty & \\
\tau^{o}\left(R_{1}\right)=\tau^{w}\left(R_{1}\right) & \frac{R_{1}}{2} \frac{\Delta p}{L}=\frac{R_{1}}{2} \frac{\Delta p}{L}+\frac{C \mu_{2}}{R_{1}} & \\
v_{z}^{w}(R)=0 & \frac{R^{2}}{4 \mu_{2}} \frac{\Delta p}{L}+D=0 & D=0 \\
v_{z}^{w}\left(R_{1}\right)=v_{z}^{o}\left(R_{1}\right) & \frac{-R_{1}^{2}}{4 \mu_{1}} \frac{\Delta p}{L}+B=\frac{-R_{1}^{2}}{4 \mu_{2}} \frac{\Delta p}{L}+\frac{R^{2} \Delta p}{4 \mu_{2} L} & B=\frac{\Delta P}{4 L}\left(\frac{R_{1}^{2}}{\mu_{1}}+\frac{\left(R^{2}-R_{1}^{2}\right)}{\mu_{2}}\right)
\end{array}
$$

Resulting on the final equations on the form of:
For oil $0 \leq r \leq R_{1}$

$$
\begin{array}{r}
v_{z}^{o}(r)= \\
\frac{-r^{2}}{4 \mu_{1}} \frac{\Delta P}{L}+\frac{\Delta P}{4 L}\left(\frac{R_{1}^{2}}{\mu_{1}}+\frac{\left(R^{2}-R_{1}^{2}\right)}{\mu_{2}}\right) \\
v_{z}^{o}(r)=\frac{\Delta P}{4 L}\left(\frac{R_{1}^{2}-r^{2}}{\mu_{1}}+\frac{R^{2}-R_{1}^{2}}{\mu_{2}}\right)
\end{array}
$$

For water $R_{1} \leq r \leq R$

$$
\begin{gathered}
v_{z}^{w}(r)=\frac{-r^{2}}{4 \mu_{2}} \frac{\Delta P}{L}+\frac{R^{2} \Delta P}{4 \mu_{2} L} \\
v_{z}^{w}(r)=\frac{\Delta P}{4 \mu_{2} L}\left(R^{2}-r^{2}\right)
\end{gathered}
$$

For oil and water $0 \leq r \leq R$

$$
\tau^{o}(r)=\tau^{w}(r)=\frac{r}{2} \frac{\Delta P}{L}
$$

The velocity on the interface is the velocity in $R_{1}$ and can be calculated using any of the velocity equations (water or oil) resulting in:

$$
v_{z}\left(R_{1}\right)=\frac{\Delta P}{4 \mu_{2} L}\left(R^{2}-R_{1}^{2}\right)
$$

Other relevant quantities are the shear stress on the wall and the maximum velocity.

$$
\tau^{w}(R)=\frac{R}{2} \frac{\Delta P}{L} \quad v_{z}^{o}(0)=\frac{\Delta P}{4 L}\left(\frac{R_{1}^{2}}{\mu_{1}}+\frac{R^{2}-R_{1}^{2}}{\mu_{2}}\right)
$$

The velocity profile resulting from the equations can be visualized in Figure 1.1.


Figure 1.1: Velocity and Shear stress profiles

## 1.6 )

To calculate the flux of each of the fluids it is necessary to integrate the velocity field over the area as following:

For oil:

$$
\begin{aligned}
& Q_{o}=\iint_{A_{1}} v_{z}^{o} d A_{1}=\int_{0}^{R_{1}} \int_{0}^{2 \pi}\left[\frac{-r^{2}}{4 \mu_{1}} \frac{\Delta p}{L}+\frac{\Delta P}{4 L}\left(\frac{R_{1}^{2}}{\mu_{1}}+\frac{\left(R^{2}-R_{1}^{2}\right)}{\mu_{2}}\right)\right] r d r d \theta \\
& Q_{o}=-\frac{r^{4} \Delta P}{16 \mu_{1} L}+\left.\frac{r^{2}}{2} \frac{\Delta P}{4 L}\left(\frac{R_{1}^{2}}{\mu_{1}}+\frac{\left(R^{2}-R_{1}^{2}\right)}{\mu_{2}}\right)\right|_{0} ^{R_{1}} 2 \pi=-\frac{2 \pi R_{1}^{4} \Delta P}{16 \mu_{1} L}+\frac{R_{1}^{2}}{2} \frac{\Delta P}{4 L}\left(\frac{R_{1}^{2}}{\mu_{1}}+\frac{\left(R^{2}-R_{1}^{2}\right)}{\mu_{2}}\right) 2 \pi \\
& Q_{o}=\frac{\pi \Delta p}{4 L}\left(\frac{R_{1}^{2}}{\mu_{2}}\left(R^{2}-R_{1}^{2}\right)+\frac{R_{1}^{4}}{2 \mu_{1}}\right)
\end{aligned}
$$

For water:

$$
\begin{aligned}
& Q_{w}=\iint_{A_{2}} v_{z}^{w} d A_{2}=\int_{R_{1}}^{R} \int_{0}^{2 \pi}\left[-\frac{r^{2} \Delta P}{4 \mu_{2} L}+\frac{R^{2} \Delta P}{4 \mu_{2} L}\right] r d \theta d r \\
& Q_{w}=\left.\left(-\frac{r^{4} \Delta P}{16 \mu_{2} L}+\frac{r^{2}}{2} \frac{R^{2} \Delta P}{4 \mu_{2} L}\right)\right|_{R_{1}} ^{R_{2}} 2 \pi=\left(-\frac{R^{4}-R_{1}^{4} \Delta P}{16 \mu_{2} L}+\frac{R^{2}-R_{1}^{2}}{2}\left(\frac{R^{2} \Delta P}{4 \mu L}\right)\right) \\
& Q_{w}=\frac{\pi \Delta p}{8 \mu_{2} L}\left(R^{2}-R_{1}^{2}\right)^{2}
\end{aligned}
$$

2 Considering the shock tube shown in Figure 2.1 with initial velocities equal to 0 :


Figure 2.1: Schematic of the problem
The Riemann invariants for the expansion and compression lines may be written as a function of the different pressures:

$$
\begin{aligned}
& \frac{u}{c}-\frac{1}{\gamma} \frac{p}{p_{o}}=\text { constant along } x+c t=\mathrm{constant} \\
& \frac{u}{c}+\frac{1}{\gamma} \frac{p}{p_{o}}=\mathrm{constant} \text { along } x-c t=\mathrm{constant}
\end{aligned}
$$

We know that those expressions remain constant along characteristic lines, therefore by knowing the initial pressure and velocity at both sides of the diaphragm, we can calculate those same quantities at a point after the wave front has passed as shown in Figure 2.2.


Figure 2.2: Wave front after the diaphragm breaks
From the points P to $\mathrm{B}(x+c t)$, knowing that $u_{b}=0$ and $p_{b}=p_{o}$

$$
\begin{gather*}
\frac{u_{p}}{c}-\frac{1}{\gamma} \frac{p_{p}}{p_{o}}=\frac{0}{c}-\frac{1}{\gamma} \frac{p_{o}}{p_{o}} \\
\frac{u_{p}}{c}=\frac{1}{\gamma}\left(\frac{p_{p}}{p_{o}}-1\right) \tag{2.1}
\end{gather*}
$$

From the points P to $\mathrm{A}(x-c t)$, knowing that $u_{a}=0$ and $p_{a}=p_{1}$

$$
\begin{equation*}
\frac{u_{p}}{c}+\frac{1}{\gamma} \frac{p_{p}}{p_{o}}=\frac{0}{c}+\frac{1}{\gamma} \frac{p_{1}}{p_{o}} \tag{2.2}
\end{equation*}
$$

Plugging (2.1) into (2.2)

$$
\frac{1}{\gamma}\left(\frac{p_{p}}{p_{o}}-1\right)+\frac{1}{\gamma} \frac{p_{p}}{p_{o}}=\frac{1}{\gamma} \frac{p_{1}}{p_{o}}
$$

We get the pressure at point P

$$
\begin{equation*}
p_{p}=\frac{p_{o}+p_{1}}{2} \tag{2.3}
\end{equation*}
$$

To find the velocity at that same point we just have to plug (2.3) into (2.1)

$$
\frac{u_{p}}{c}=\frac{1}{\gamma}\left(\frac{p_{o}+p_{1}}{2 p_{o}}-1\right)
$$

The final expression for velocity at point P is:

$$
\begin{equation*}
u_{p}=\frac{c}{2 \gamma}\left(\frac{p_{1}}{p_{o}}-1\right) \tag{2.4}
\end{equation*}
$$

To find the pressure and velocity after the wave hits the wall it is ncessary first to find the pressure on the wall as shown in the Figure 2.3, remarking that the $u_{w}=0$.


Figure 2.3: Wave front after it hits the wall and characteristic lines
From the points W to $\mathrm{P}(x-c t)$

$$
\begin{equation*}
\frac{0}{c}+\frac{1}{\gamma} \frac{p_{w}}{p_{o}}=\frac{u_{p}}{c}+\frac{1}{\gamma} \frac{p_{p}}{p_{o}} \tag{2.5}
\end{equation*}
$$

We can plug (2.3) into (2.5)

$$
\frac{0}{c}+\frac{1}{\gamma} \frac{p_{w}}{p_{o}}=\frac{1}{2 \gamma}\left(\frac{p_{1}}{p_{o}}-1\right)+\frac{1}{\gamma} \frac{p_{o}+p_{1}}{2 p_{o}}
$$

To get the pressure at the wall

$$
\begin{equation*}
p_{w}=p_{1} \tag{2.6}
\end{equation*}
$$

The only remaining pressure and velocities unknown are $p_{q}$ and $u_{q}$, when the wave bounces against the wall and comes back. To find them we use the characteristic lines that pass through points Q-P and Q-W.

From point P to $\mathrm{Q}(x-c t)$

$$
\begin{equation*}
\frac{u_{p}}{c}+\frac{1}{\gamma} \frac{p_{p}}{p_{o}}=\frac{u_{q}}{c}+\frac{1}{\gamma} \frac{p_{q}}{p_{o}} \tag{2.7}
\end{equation*}
$$

Plugging (2.3) and (2.4) into (2.7) we get:

$$
\begin{equation*}
\frac{1}{2 \gamma}\left(\frac{p_{1}}{p_{o}}-1\right)+\frac{1}{\gamma} \frac{p_{o}+p_{1}}{2 p_{o}}=\frac{u_{q}}{c}+\frac{1}{\gamma} \frac{p_{q}}{p_{o}} \tag{2.8}
\end{equation*}
$$

From point Q to W $(x-c t)$

$$
\frac{u_{q}}{c}-\frac{1}{\gamma} \frac{p_{q}}{p_{o}}=\frac{u_{w}}{c}-\frac{1}{\gamma} \frac{p_{w}}{p_{o}}
$$

We know that $u_{w}=0$ and $p_{w}=p_{1}$

$$
\begin{equation*}
\frac{u_{q}}{c}-\frac{1}{\gamma} \frac{p_{q}}{p_{o}}=-\frac{1}{\gamma} \frac{p_{1}}{p_{o}} \tag{2.9}
\end{equation*}
$$

We have got a linear system of equations formed by (2.8) and (2.9) with $p_{q}$ and $u_{q}$ as unknowns. If we solve it we get:

$$
p_{q}=p_{1} \quad u_{q}=0
$$

As a summary, we can identify 4 regions in the space-time domain as shown in Figure 2.4 and Table 2.1.


Figure 2.4: Pressure and velocity space-time regions

Table 2.1: Summary

|  | a | b | c | d |
| :---: | :---: | :---: | :---: | :---: |
| velocity | 0 | 0 | $\frac{c}{2 \gamma}\left(\frac{P_{1}}{P_{0}}-1\right)$ | 0 |
| pressure | $P_{1}$ | $P_{0}$ | $\frac{P_{1}+P_{0}}{2}$ | $P_{1}$ |

Looking at the graph, it is clear that for a big enough time the pressure and velocity are going to be the same as region $d$ of Figure 2.4.

