ADVANCED FLUID MECHANICS

HOMEWORK ASSIGNMENT 2

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ASSIGNMENT NO.2

1) Assumptions

Flow is considered as in constant density

- (ii) inviscid.
- (iii) Steady

Applying mass balance for r/a.

$$Q = \pi a^2 V = 2\pi h v r$$

$$Vr = \frac{q^2 V}{2hr} = C_1 = \frac{a^2 V}{2h}$$

When r=a. mass balance is

$$C_1 a = \frac{a^2 V}{2ha} \Rightarrow C_1 = \frac{V}{2h}$$

$$\begin{bmatrix} a^2 C_1 = C_2 \end{bmatrix}$$

(b) Estimating pressure Field

Applying Bernoulli at PQR streamline.

$$so_{p(r)} - po = p(r) + 12p[v_r^2 - v_o^2]$$

FT=
$$\frac{1}{2}\pi\rho v^{2}\left[r^{2}-\frac{r^{4}}{8h^{2}}\right]^{2}$$
 $\frac{1}{2}\pi\rho v^{2}\left[r^{2}a-\frac{a^{4}}{2h^{2}}+n(r)\right]^{2}a$
 $=\frac{1}{2}\pi\rho v^{2}\left[\alpha^{2}-\frac{a^{4}}{8h^{2}}+R^{2}-a^{2}-\frac{a^{4}}{2h^{2}}\ln(R)\right]^{2}$
 $=\frac{1}{2}\pi\rho v^{2}\left[R^{2}-\frac{a^{4}}{8h^{2}}+\frac{a^{4}}{2h^{2}}\ln(\frac{R}{a})\right]^{2}$
 $=\frac{1}{2}\pi\rho v^{2}\left[R^{2}-\frac{a^{4}}{8h^{2}}+\frac{a^{4}}{2h^{2}}\ln(\frac{R}{a})\right]^{2}$

In Abore expression, first term is always negative because $\frac{1}{2}$ and $\frac{1}{2}$ will be negative when $\frac{1}{2}$ and $\frac{1}{2}$ will be negative when $\frac{1}{2}$ and $\frac{1}{2}$ will be $\frac{1}{2}$ and $\frac{1}{2}$ will be $\frac{1}{2}$ and $\frac{1}{2}$ and

Under giren condition

Fr = - W

Pair = 1.2 Kg/m2

 $\alpha = 10^{-2} \text{m}.$

P=1.2 Kg/m3.

R = 5 E-2m

h = 0.1E-2m

W = mg = (10E-3)(9.8) = 9.8E-3.N

plugging these values in the

following equation.

$$-W = \frac{1}{2} \pi P V^{2} \left[R^{2} - \frac{\alpha^{4}}{8h^{2}} + \frac{\alpha^{4}}{2h^{2}} \left(\frac{\alpha}{R} \right) \right]$$

V= 2.78m/S

(d) Unsteady Flow Condition

a Mays + Emout + min

JPW-VO. ROA

 $\frac{d}{dt}\left(\frac{drh}{dt}\right) - \frac{d}{dt}\left(\frac{drh}{dt}\right) = 0$

POTERTIED & mout + min = dM

$$\frac{dN}{dT} = PV_{r}^{2} \pi rh - pVa^{2}\pi + p\pi rh(t) = 0$$

$$Vr = \frac{Va^{2}}{2rh} - \frac{r^{2}h(t)}{2rh}$$
This expression is only ratio real bout for real date to the notwine

For a a

$$Va^{2} - a^{2}h^{2} = C_{1}$$

$$2ah$$

$$C_{1} = \frac{V - h(t)}{2h}$$

$$V_{r} = \begin{cases} \frac{(V - h)r}{2h} & r \neq 0 \end{cases}$$

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$$\int_{0}^{R} \frac{d}{dt} \left(\frac{V_{ir} - h(t)r}{2r} \right) dr + \int_{0}^{R} \frac{d}{dt} \left(\frac{V_{ir} - h(t)r}{2rh} \right) dr$$

$$+ \int_{0}^{R} \left(\frac{V_{ir} - h(t)r}{2rh} \right) dr + \int_{0}^{R} \frac{d}{dt} \left(\frac{V_{ir} - h(t)r}{2rh} \right) dr$$

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$$+ \int_{0}^{R} \left(\frac{V_{ir} - h(t)r}{2rh} \right) dr$$

(2) Solution > cylindrical lin Laptacian Polar coordinato wo hare the Following expression for Laplacian of Scalar Field $\nabla^2 a = \frac{\partial^2 a}{\partial r^2} + \frac{1}{r} \frac{\partial a}{\partial r} + \frac{1}{r^2} \frac{\partial^2 a}{\partial \theta^2}$ U(r, e) = 7(r) sin & with f(r)= xx. $\Psi(r, \theta) = r^{\alpha} \sin \theta$ 724 - 324 + 1 325 + 1 326, 3r2 + 1 375 + 1 30° $\sqrt{y} = (\alpha^2 - \alpha) r^{\alpha - 2} \sin \theta + \pm \alpha r^{\alpha - 1} \sin \theta - \frac{\alpha^{-2}}{r} \sin \theta$ $\nabla^2 \Psi = \frac{1}{2} \operatorname{Sin} \Theta \left(\alpha^2 - 1 \right)$ we have For flow to be irrotational 724=0

So our streamline function is $V = \alpha \sin \theta + b r \sin \theta$

$$Vr = \frac{1}{r} \frac{\partial Ur}{\partial \theta}$$

$$Vr = \frac{1}{r} \left(\frac{\alpha_{1} \cos \theta}{r} + \frac{\alpha_{1} \cos \theta}{r} \right)$$

$$Vr = \frac{\alpha_{1} \cos \theta}{r^{2}} + \frac{\alpha_{2} \cos \theta}{r^{2}}$$

$$V\theta = \frac{\partial Ur}{\partial r}$$

$$= -\left(-\frac{\alpha_{1} \sin \theta}{r^{2}} + \frac{\alpha_{2} \sin \theta}{r^{2}} \right)$$

$$V\theta = \frac{\alpha_{1} \sin \theta}{r^{2}} + \frac{\alpha_{2} \sin \theta}{r^{2}}$$

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Applying Boundary conditions now

Second Boundary condition

$$Vr = \frac{4 \text{ ay } \cos \pi}{R^2} + b \cos \pi$$

$$Vr = -\frac{\alpha \theta}{R^2} - Ux$$

$$O = -\frac{\alpha \theta}{R^2} - Ux$$

$$QA = -Ux$$

$$Vr = \frac{1}{2} \frac{\partial U}{\partial \theta} = -\frac{1}{2} \frac{2}{x} \frac{\partial U}{\partial \theta} + \frac{1}{2} \frac{1}{x} \cos \theta$$

$$Vr = \frac{1}{2} \frac{\partial U}{\partial \theta} = -\frac{1}{2} \frac{1}{x} \frac{1}{x} \cos \theta$$

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$$V = -\frac{1}{2} \frac{1}{x} \frac{1}{x} \cos \theta$$

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$$VO = -U_X Sin O \left[1 + R^2 \right]$$

At r=R we have the following Boundary conditions Vr=0, Vo-- ZUXSino Our stream line function for is U= (Fdy) + (Dy) = Ux Our V= R VA-=0 (c) Velocity Field W= 1 V2+ V0-Ve = -2 Ux Sino M = 1 44x2 Sinze V=14Ux' Sno Applying the Bernoullis theorem on streamline AB (Note B Lies on the cylindersirface) PA + 1 P VA = P2 + 1 P VB2 P1 + 1 PU = P2. + 1 (P (2U Sin E)2 Pr - Pr = #PU[2sin28-1] P1-P2 , U2P [(cs 20 - 1]

NET FORCE ACTING ON CYLINDER

FH =
$$\sqrt{\frac{2\pi}{3}}$$
 PR $\sqrt{\frac{2\pi}{3}}$ PR

FH =
$$PU^{2}R[-\frac{1}{2}Sin\Theta]^{2}$$

FH = O
*TO
FV - $U^{2}PR[(OS2\Theta-1]Sin\Theta]$ de
= $U^{2}PR[(OS2\Theta-1]Sin\Theta]$ de
 $Sin(-\Theta) = -Sin\Theta$
 $Cos(-\Theta) = -Cos\Theta$
= $U^{2}PR[-\frac{\pi}{2}(Cos2\Theta-1)Sin\Theta]$ + $\int (Cos2\Theta-1)Sin\Theta$ do
So Net force $F = \int FY^{2} + FP^{2}$

Discussion

Un practice we should get a drag but in this case as we have solved stroam lines for in ampressible flow, in so there would be no viscosity in Ita Constitutive relation and premure on both side of cylinder is even. So our drag will be Copial to O